

U.S. Serial No. 10/652,345
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AMENDMENTS TO THE CLAIMS

Claim 1. (cancelled)

Claim 2. (currently amended) The process of claim ~~1~~ 15 wherein the catalyst deactivation rate, as measured by temperature increase required to meet a predetermined pour or cloud point (TIR) is less than 25°F/year (14°C/year).

Claim 3. (cancelled)

Claim 4. (currently amended) The process of claim ~~3~~ 15 wherein the hydrogen partial pressure is less than about 70 psig (584 kPa).

Claim 5. (cancelled)

Claim 6. (currently amended) The process of claim ~~5~~ 4 wherein the dehydrogenation component is platinum or palladium.

Claims 7 and 8. (cancelled)

Claim 9. (currently amended) The process of claim ~~8~~ 15 wherein catalyst regeneration is effected by hydrogen stripping or oxygen treatment.

Claim 10. (currently amended) The process of claim ~~5~~ 15 wherein the product of the catalytic dewaxing process is a lube base stock or a diesel range material.

Claim 11. (original) The process of claim 10 wherein the product is subjected to hydrofinishing.

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Claim 12. (original) The process of claim 11 wherein the molecular sieve is selected from the group consisting of ZSM-23, ZSM-35, ZSM-48, ZSM-22, SSZ-32, zeolite beta, mordenite, rare earth ion exchanged ferrierite and mixtures thereof.

Claim 13. (original) The process of claim 12 wherein the molecular sieve is ZSM-48.

Claim 14. (original) Use of the process according to claim 13 to (1) decrease the pour point or cloud point, or both, and (2) preserve the viscosity of a paraffin containing feed stock.

Claim 15. (new) A cyclic catalytic dewaxing-catalyst regeneration process which comprises: catalytically dewaxing a paraffin containing feed stock in a first reaction zone for a predetermined period after which the catalytic dewaxing of the paraffin containing feed stock is conducted in a second reaction zone for a predetermined period and the catalyst in the first reaction zone is regenerated after which the paraffin containing feed is dewaxed in the first reaction zone and the catalyst in the second zone is regenerated; and wherein the paraffin containing feed stock contains greater than 80 wt% n-paraffins and has a boiling point above about 430°F (221.1°C); wherein the catalyst in the first and second zone comprises a molecular sieve with a one dimensional pore structure having an average diameter of 0.50 to 0.65 nm and a metal dehydrogenation component; and, wherein the catalyst dewaxing is conducted at dewaxing conditions and in the substantial absence of added hydrogen and at a hydrogen partial pressure of less than about 100 psi (791 kPa).